

7.6 Flow Across Banks of Tubes

Fundamentals of Heat and Mass Transfer, 8th Edition

Table for C and M values

TABLE 7.5 Constants of Equation 7.58 for the tube bank in cross flow [17]

Configuration	$Re_{D,\max}$	C_1	m
Aligned	$10-10^2$	0.80	0.40
Staggered	$10-10^2$	0.90	0.40
Aligned	10^2-10^3	Approximate as a single (isolated) cylinder	0.63
Staggered	10^2-10^3		
Aligned ($S_T/S_L > 0.7$)*	$10^3-2 \times 10^5$	0.27	0.63
Staggered ($S_T/S_L < 2$)	$10^3-2 \times 10^5$	$0.35(S_T/S_L)^{1/5}$	0.60
Staggered ($S_T/S_L > 2$)	$10^3-2 \times 10^5$	0.40	0.60
Aligned	$2 \times 10^5-2 \times 10^6$	0.021	0.84
Staggered	$2 \times 10^5-2 \times 10^6$	0.022	0.84

*For $S_T/S_L < 0.7$, heat transfer is inefficient and aligned tubes should not be used.

Table for C and M coefficients.

$$\overline{Nu}_D = C_1 Re_{D,\max}^m Pr^{0.36} \left(\frac{Pr}{Pr_s} \right)^{1/4}$$

$$\left[\begin{array}{l} N_L \geq 20 \\ 0.7 \lesssim Pr \lesssim 500 \\ 10 \lesssim Re_{D,\max} \lesssim 2 \times 10^6 \end{array} \right]$$

At least 20 tubes(**5 not 20 need correction factor**)

TABLE 7.6 Correction factor C_2 of Equation 7.59 for $N_L < 20$ ($Re_{D,\max} \gtrsim 10^3$) [17]

N_L	1	2	3	4	5	7	10	13	16
Aligned	0.70	0.80	0.86	0.90	0.92	0.95	0.97	0.98	0.99

Prandlt number range, Reynolds number range

The Reynolds number $Re_{D,\max}$ for the foregoing correlation is based on the *maximum* velocity occurring within the tube bank, $Re_{D,\max} = \rho V_{\max} D / \mu$. For the aligned arrangement, $V_{\max}$ occurs at the transverse plane A_1 of Figure 7.12a, and from the mass conservation requirement for a constant density fluid

$$V_{\max} = \frac{S_T}{S_T - D} V \quad (7.60)$$

Input vector creation and graphing

```
AirSpeed = 0:0.1:10;
tempLow = 40+ 273.15;
battTemp = 50+ 273.15;
tempHigh = 42.57 + 273.15;
%y = Heatloss(AirSpeed,tempLow,battTemp)
```

```

hold on
ylabel('HeatLoss[w]');
plot(AirSpeed,y, '.')
%yyaxis right
%plot(z,AirSpeed, '.')
xlabel('AirSpeed at Entrance [m/s]');
ylabel('Ploss');
var2 = battTemp-273.15;
var1 = tempHigh-273;
title_string = sprintf("AirSpeed Vs Heatloss at Ambient %.2f C and Battery Temp %.2f",var1,var2)

```

```

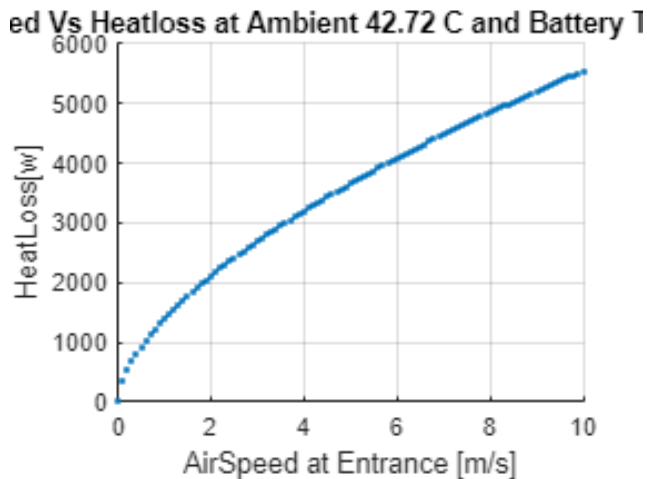
title_string =
"AirSpeed Vs Heatloss at Ambient 42.72 C and Battery Temp 50.00"

```

```

title(title_string)
grid on;
hold off

```



```

%function HeatLoss = Heatloss(AirSpeed,tempLow,battTemp)

```

Basic

```

%Reynolds Number Calcs
BattColumns = 5;
BatteryRows =23;

```

```
tempHigh = 40 + 273.15;
DiameterCells = 18.3/1000; % CHANGE THIS BECAUSE NO GAP
```

```
dynViscosity = py.CoolProp.CoolProp.PropsSI('V', 'T', tempLow, 'P|not_imposed',
101325, 'air')
```

```
dynViscosity = 1.9165e-05
```

```
densityAir = py.CoolProp.CoolProp.PropsSI('D', 'T', tempLow, 'P|not_imposed',
101325, 'air')
```

```
densityAir = 1.1274
```

```
thermCond = py.CoolProp.CoolProp.PropsSI('L', 'T', tempLow, 'P|not_imposed',
101325, 'air')
```

```
thermCond = 0.0274
```

```
ConstPNum = py.CoolProp.CoolProp.PropsSI('C', 'T', tempLow, 'P|not_imposed',
101325, 'air')
```

```
ConstPNum = 1.0069e+03
```

```
thermMassAir = py.CoolProp.CoolProp.PropsSI('C', 'T', tempLow, 'P|not_imposed',
101325, 'air')
```

```
thermMassAir = 1.0069e+03
```

```
PrandtlAirLow = py.CoolProp.CoolProp.PropsSI('Prandtl', 'T', tempLow, 'P|
not_imposed', 101325, 'air')
```

```
PrandtlAirLow = 0.7055
```

```
PrandtlAirHigh = py.CoolProp.CoolProp.PropsSI('Prandtl', 'T', tempHigh, 'P|
not_imposed', 101325, 'air')
```

```
PrandtlAirHigh = 0.7055
```

```
KinViscosity = dynViscosity/densityAir;
```

```
% Vert vs Horiz Spacing
```

```
St = 24.3/1000;% spacing between columns
```

```
Sl = 34.3/1000;%center spacing in direction of initial airflow
```

```
Vmax = St.*AirSpeed./(St-DiameterCells);
```

```
ReynoldsNumber = Vmax * DiameterCells / KinViscosity % WILL have to update C1
and M Manually before IF statements.
```

```
ReynoldsNumber = 1x101
```

```
104 ×
```

0 0.0436 0.0872 0.1308 0.1744 0.2180 0.2616 0.3052 ...

```
C1 = 0.35*(St/S1)^(1/5);
mVal = 0.6; % Table
C2 = 0.95; %Table (correction factor for 5)
```

$$\overline{Nu}_D = C_2 C_1 Re_{D,\max}^m Pr^{0.36} \left(\frac{Pr}{Pr_s} \right)^{1/4}$$

$$\bar{h} = \overline{Nu}_D \frac{k}{D} :$$

```
NusseltD = C2*C1*ReynoldsNumber.^mVal.*(PrandtlAirLow.^0.36).*(PrandtlAirLow./
PrandtlAirHigh).^(0.25);
Hline = NusseltD*thermCond/DiameterCells;
```

Adjusted Delta for warming

$$\Delta T_{lm} = \frac{(T_s - T_i) - (T_s - T_o)}{\ln \left(\frac{T_s - T_i}{T_s - T_o} \right)}$$

$$\frac{T_s - T_o}{T_s - T_i} = \exp \left(- \frac{\pi D N \bar{h}}{\rho V N_T S_T c_p} \right)$$

$$T_s - T_o = (T_s - T_i) \exp \left(- \frac{\pi D N \bar{h}}{\rho V N_T S_T c_p} \right)$$

```
insideVarTop = (-pi*DiameterCells*(BattColumns*BatteryRows)*Hline);

insideVarBot = (densityAir.*AirSpeed.*(BatteryRows)*St*ConstPNum);
adjDelTso = (battTemp - tempLow) * exp(insideVarTop/insideVarBot);
To = -((battTemp - tempLow) * exp(insideVarTop/insideVarBot))+battTemp -273.15
```

To = 42.5796

$$\Delta T_{lm} = \frac{(T_s - T_i) - (T_s - T_o)}{\ln\left(\frac{T_s - T_i}{T_s - T_o}\right)}$$

```
deltTlm = ((battTemp-tempLow)-(adjDelTso))/(log((battTemp-tempLow)/
(adjDelTso)));
```

$$q' = N(\bar{h}\pi D\Delta T_{lm})$$

```
qPrime = (BatteryRows*BattColumns)*(Hline*pi*DiameterCells*deltTlm);%in KW per m
qPrimeLadjust = qPrime*0.065*6%Temp dissapated
```

```
qPrimeLadjust = 1x101
```

```
103 ×
```

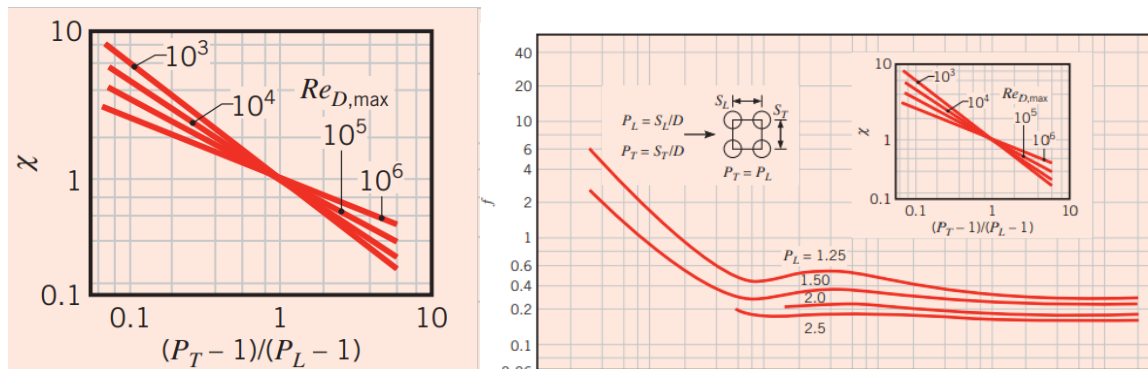
```
0    0.3498    0.5301    0.6761    0.8035    0.9186    1.0248    1.1241 ...
```

```
areaPath = St*BattColumns*0.065;
```

pressure loss

$$\Delta p = N_L \chi \left(\frac{\rho V_{max}^2}{2} \right) f$$

```
Pt = St/DiameterCells;
Pl = Sl/DiameterCells;
PTPL = (Pt-1)/(Pl-1);
```



```
fancyX = 1.4;
```

```
fricFactor = 0.22;
```

```
deltPloss = 5.* fancyX .* (densityAir./2.*Vmax.^2) .* fricFactor;
```

```
HeatLoss = qPrimeLadjust;
```

%end